

Energy Exergy Analysis of a high pressure Claude Haylentsystem for liquefaction of Gases

Devender Kumar^{*}, R. S. Mishra

Department of Mechanical Engineering, Delhi Technological University, Delhi, India

Article Info

Article history:

Received 20 July 2014

Received in revised form

10 August 2014

Accepted 20 August 2014

Available online 15 September 2014

Keywords

Thermodynamics Analysis Claude

Haylentsystem,

Energy-Exergy Analysis,

First and second Law Analysis

Abstract

From various Cryogenics systems, lot of a detailed thermodynamic analysis of cryosystems have been reported in literature however the modification of Claude systems for high pressure for high yield of liquefied mass of gases is very limited available in literature so far. A comprehensive energy and exergy analysis of Claude Heylandcryogenic system for various gases is carried out in this paper by using various properties variables (i.e temperature, pressure etc) in system to find out the more efficient statics of system included exergy destructions in system. Numerical computations have been carried out for various gases in Claude Haylent system and it was observed that the Methane gas is more suitable than any other observed gas and 350 and 500 bar is best compressor pressure per kg of inlet gas.

Nomenclature

M	=	Total mass of gas
m_f	=	liqified mass of gas
m_4	=	mass of air in second heat exchanger
m_8	=	mass of air liquefied in the separator
h	=	Enthalpy
S	=	Entropy
X	=	Dryness fraction
T	=	temperature
P	=	Pressure
η_{comp}	=	Efficiency of compressor (approx. 80%)
$\eta_{expander}$	=	Efficiency of expander (approx. 80%)
$\eta_{2nd\ law}$	=	Second law efficiency
ϵ	=	Effectiveness of heat exchanger (approx. 80%)
C	=	Specific heat capacity fluid or gas
W_t	=	Work of reversible isothermal compression
W_c	=	Shaft work supplied to compressor per unit mass
R	=	Universal gas constant
W_{net}	=	Net work done in system

1. Introduction

Cryogenic engineering is the application of low temperatures in which operating temperature below $-150\text{ }^\circ\text{C}$. Various gases like air, nitrogen, argon are liquefied. First vapour compression systems are used to achieve cryogenic temperature but used of these system worked is limited due to solidification temperature of the refrigerants. After this cryogenic industry find number of modes to achieve low temperature. Several liquefaction cycles exist [1]. Various processes are design and invent to achieve cryo temperature

Corresponding Author,

E-mail address: devenderdahiya@in.com

All rights reserved: <http://www.ijari.org>

at different level of lower temperature Cryogenics is used in various important process at different level with different naming like cryobiology, cryonics, cryo-electronics, cryotrons, cryosurgery etc. Claude system is one of cryogenic system which is design to liquefy various particular gases like air, oxygen, nitrogen, feronetc. To improve performance of Claude system its modification is done in form of Haylentsystem. Haylent system is high pressure side Claude system but still Liquefaction plants are rather complicated with numerous components interacting with each other and consume a large amount of process energy, it is vital to develop efficient liquefaction processes for improving the overall system performance and economic competitiveness [2]. Various research and different method are employed to increase efficiency of cryo system. Exergy analysis is a strong method to identified inefficiencies of system and tells which part of system is critical and need to to be undertake study. From literature various data collected which help in optimization of cryosystem. The Bejan [3] work is bse of all exergetic analysis of heat exchangers. Various problems are studied related to exergy analysis which are mentioning or summarized in [4], from the vast study it noticed that most new methods differ only in the way that entropy generation is non-dimensional [5]. A good exergetic design of a heat exchanger would allow for an increase in the global efficiency of the process, by defining a thermodynamic cycle in which the exergetic losses would be limited [6]. The major cause of exergy loss is the use of compressors and to a lesser extent the use of turbines [7]. For optimization of Haylent system first and second law analysis is done but except to increase the whole Haylent system efficiency stress are done on particular parts of system and research are done on that systems. Air separation unit and compressor, condenser and evaporator of cryo system are the center of research because most of exergy destruction takes place in these parts. This paper mainly dealt with thermodynamic (exergy and anergy) analysis of Haylent system for determining the effect of every component of system with varying conditions for maximum second law efficiency

2. Thermo Analysis of Claude Haylent System for Liquefaction of Gases

Compressor work:

$$\eta_c = \frac{W_t}{W_{comp}} \tag{1}$$

$$W_c = mRT \ln \frac{P_2}{P_1} \tag{2}$$

$$-W_c = m * (T_1 * (s_1 - s_2) - (h_1 - h_2)) \tag{3}$$

$$W_{reversible} = W_{actual} - T_0 S_{gen} \tag{4}$$

$$W_{net} = W_c + W_e \tag{5}$$

Expander:

$$\frac{T_3}{T_2} = \left(\frac{P_3}{P_2}\right)^{\left(\frac{\gamma-1}{\gamma}\right)\eta_{expander}} \tag{6}$$

$$W_e = m_e * h_2 - m_e * h_e$$

"Control volume except compressor"

$$y = \frac{(h_1 - h_2)}{(h_1 - h_f)} + r * \frac{(h_2 - h_e)}{(h_1 - h_f)}$$

$$y = m_f / m$$

"Work done per mass of gas"

$$z = -W_{net} / m$$

"Work done per mass of liq gas"

$$t = -W_{net} / m_f$$

Coefficient of performance of system

$$COP = \frac{(h_1 - h_f)}{W_{net}}$$

Second law analysis:

$$\eta_{2nd\ law} = \frac{((h_f - h_1) - T_0 * (s_f - s_1))}{(W_{net}) * m_f} * 100$$

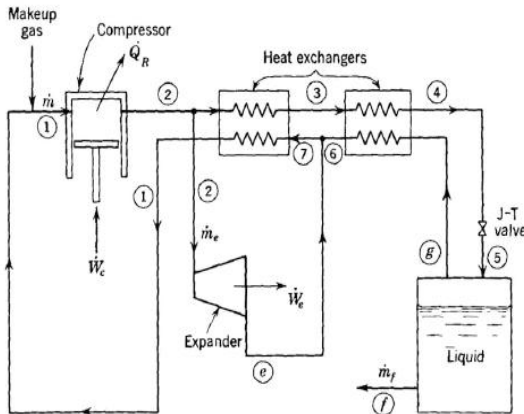


Fig. 1. Block Diagram of Haylent System

A complete analysis of Haylent Claude cycle is performing with the help of numerical computation technique for various gases. Haylent Claude cycle as shown in Fig 1 is taken for analysis. Haylent Claude system is almost same as simple Claude system except arrangement of first expander. In Haylentsystem expander intake is at high pressure side before first initial heat exchanger other than this it also consist a compressor, expander, two heat exchangers with throttle valve and separator. The fluids which have to liquefy first fed to compressor in its gaseous

form at atmospheric pressure and temperature which circulate from all system and in last fractional mass of total mass get liquefied and remaining again fed in system with additional mass to recirculate in system again. Various results are drawn for particular inlet temperature, pressure and intermediate pressure for high pressure side of expander for different six type gases such oxygen, argon, methane, air, fluorine and nitrogen are considered for study.

3. Results and Discussion

Various results are drawn on the basis of numerical equations of system. In fig 2 variation of liquefaction temperature is directly proportional to inlet pressure as we increases the pressure Liquefaction temperature raises. Fig 3 show fall of liquefaction mass with increase of inlet temperature where as fig 4 shows first incresse of liquification mass with increase of inlet pressure but after 3.5 bar it start decreasing, but this decrement with increase of inlet pressure is very slow. Fig 5-7 show variation in second law efficiency with inlet temperature, intermediate mass and inlet pressure respectively. Graph analysis of these 5-7 fig shows that second law efficiency is decreses with (increase of inlet temperature and intermediate mass whereas it is increses with increase of inlet pressure. Fig 8 -9 show variation in COP of system with inlet pressure and temperature. They show that increase in pressure is desirable for system and COP of system is increses with (increase in inlet pressure while it is decresing with increase in inlet temperature. From above graph study it determined that increses in inlet pressure is between 3 and 4 bar is (desriable for system and increase in temperature in very concern reange is good for optimization of Haylentclaude system.

(8)

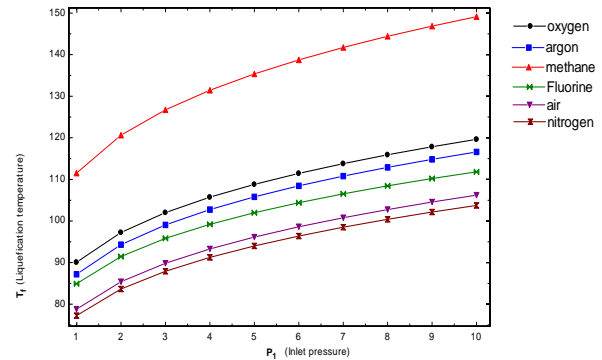


Fig. 2. Variation of liquefaction temperature with inlet Pressure

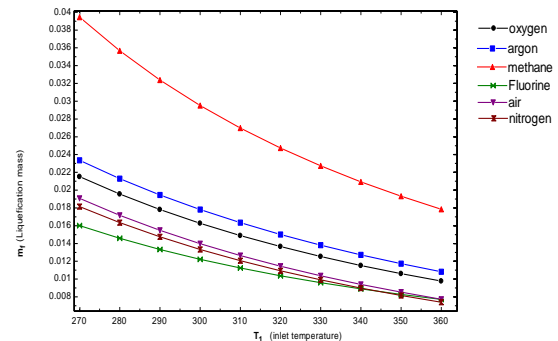


Fig. 3. Variation of Liquefied Mass with Inlet Temperature

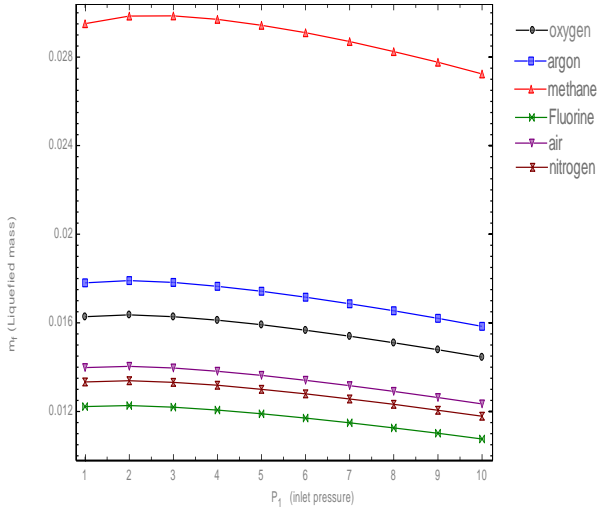


Fig. 4. Variation of Liquefied Mass with Inlet Pressure

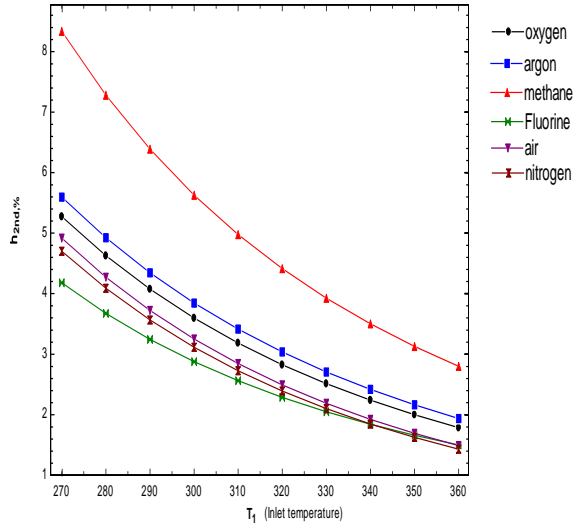


Fig. 5. Variation of 2nd law Efficiency with Inlet Temperature

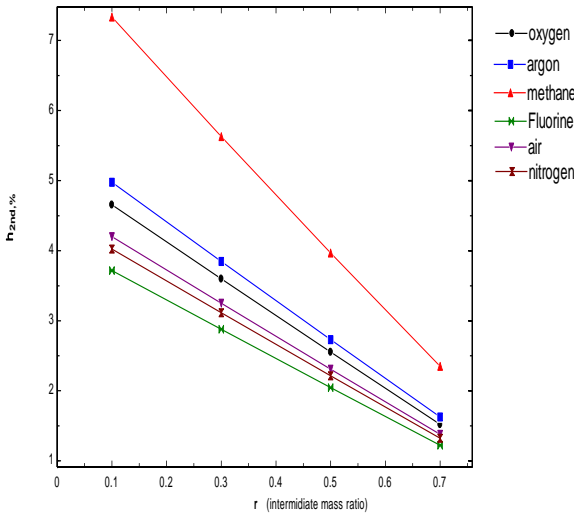


Fig. 6. Variation of 2nd law Efficiency with Intermediate Mass Ratio

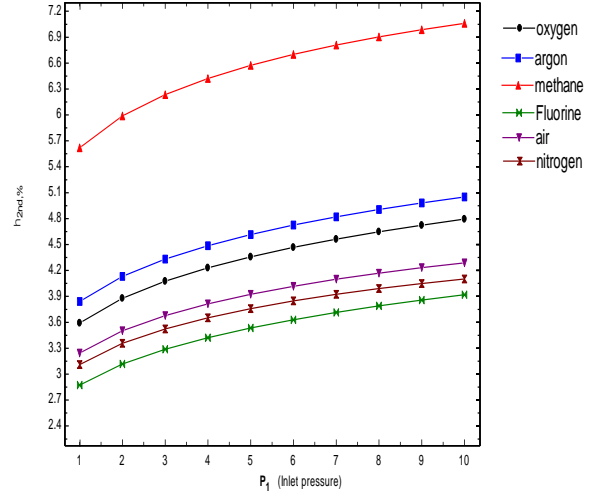


Fig. 7. Variation of 2nd law Efficiency with Inlet Pressure

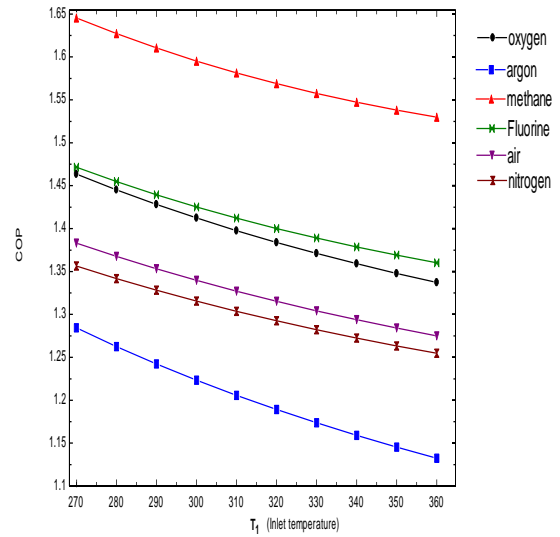


Fig. 8. Variation of COP with Inlet Temperature

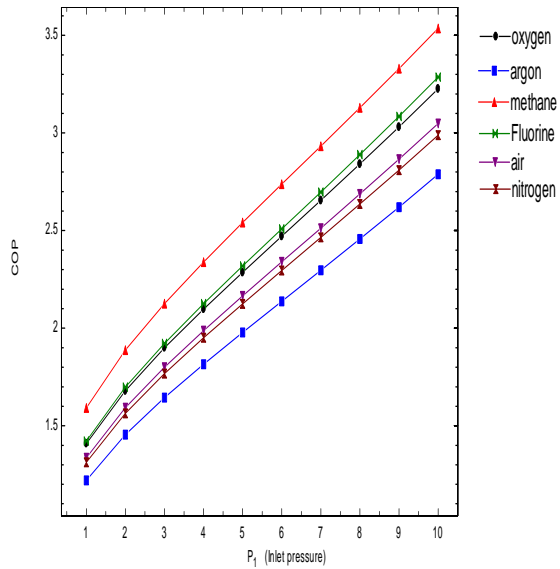


Fig. 9. Variation of COP with Inlet Pressure

4. Conclusion

From above study following results are concluded

1. The optimize range of inlet pressure is 3 .5 bar for considered variables such liquefaction mass, liquidation temperature and second law efficiency.
2. Intermediate pressure of high pressure side expander should be in minimum range for high second law efficiency.

3. Increase in inlet temperature deteriorate the performance of system and various Like COP, second law efficiency ,liquefaction mass are decrease with increase in inlet temperature

References

- [1] G. Venkatarathnam, Cryogenic Mixed Refrigerant Processes, New York, 2008
- [2] M. Kanoglu, Cryogenic turbine efficiencies. Exergy, Int J 2001; 1: 202–8
- [3] A. Bejan, General criterion for rating heat-exchanger performance. Int. J. Heat Mass Transf. 1978, 21, 655–658
- [4] M. Yilmaz, O. N. Sara, S. Karsli, Performance evaluation criteria for heat exchangers based onsecond law analysis. Exergy Int. J. 2001, 4, 278–294
- [5] S. T. Wu, X. F. Yuan, Y. R. Li, L. Xiao, Exergy transfer effectiveness on heat exchanger for finitepressure drop. Energy 2006, 32, 2110–2120.
- [6] T. J. Kotas, The Exergy Method of Thermal Plant Analysis; 1995 Ed.; Krieger Publishing Company:London, UK, 1985
- [7] R. L. Cornelissen, G. G. Hirs, Exergy analysis of cryogenic air separation, Energy Conversion and Management, 39, 16–18, 1998, 1821-1826